

IN THE CLAIMS:

Please cancel claims 25 and 29 without prejudice.  
Please amend claims 23 and 43 to recite the features of  
canceled claims 25 and 29.

Claims 1 to 22. (Canceled).

Claim 23. (Currently Amended).

A process for producing monolithic supported catalysts  
for gas-phase oxidation comprising

coating a catalyst support with a suspension,  
wherein the suspension comprises catalytically  
active composition comprising at least one type of  $TiO_2$  and  
1-10% by weight of at least one surfactant of the formula



where R is a hydrophobic group of the surfactant and n is 1,  
2 or 3; Y is a hydrophilic group of the surfactant and m is  
0, 1, 2 or 3, and X is a hydrophilic head group of the  
surfactant; and the percent by weight is based upon the total  
weight of the composition;

wherein the head group X present in the surfactant is a  
functional group selected from the group consisting of

carboxylate, polycarboxylate, phosphate, phosphonate, sulfate and sulfonate; and

wherein hydrophobic groups R of the surfactant used are selected from the group consisting of saturated alkyl radicals with carbon building blocks having from 5 to 30 carbon atoms, unsaturated alkyl radicals with carbon building blocks having from 5 to 30 carbon atoms; and

branched alkyl radicals with carbon building blocks having from 5 to 30 carbon atoms and are bound either directly or via aryl groups to a group selected from the group consisting of the hydrophilic group Y and the head group X.

Claim 24. (Previously Presented).

The process as claimed in claim 23,  
wherein the surfactant comprises from 2 to 5% by weight based upon the total weight.

Claim 25. (Canceled).

Claim 26. (Currently Amended).

The process as claimed in claim ~~25~~, 23,

wherein at least one of the functional groups of the head group X is selected from the group consisting of free acid group, ammonium salt, and alkaline earth metal salt.

Claim 27. (Previously Presented).

The process as claimed in claim 23,

wherein the hydrophilic group Y is bound to a central atom of the head group X either directly or via an oxygen.

Claim 28. (Previously Presented).

The process as claimed in claim 23,

wherein the hydrophobic group R of the surfactant used is bound to the head group X via a hydrophilic group Y.

Claim 29. (Canceled).

Claim 30. (Previously Presented).

The process as claimed in claim 23,

wherein the hydrophilic group Y of the surfactants used comprises polymeric alkoxy units whose degree of polymerization is from 1 to 50 monomer units.

Claim 31. (Previously Presented).

The process as claimed in claim 23,

wherein said at least one surfactant is selected from the group consisting of calcium alkylarylsulfonate, alkylphenol ethoxylate, ammonium alkylarylsulfonate, calcium dodecylbenzenesulfonate, polyethoxy (dinonyl phenyl ether phosphate), polyoxoethylene (lauryl ether phosphate), polyethoxy (tridecyl ether phosphate), calcium dodecylbenzenesulfonate, tridecyl phosphate ester, ethoxylated phosphated alcohol, alkyl polyoxyethylene ether phosphate, and ammonium nonyl phenyl ether sulfate.

Claim 32. (Previously Presented).

The process as claimed in claim 23,

wherein the catalytically active composition further comprises  $V_2O_5$  as an additional component.

Claim 33. (Previously Presented).

The process as claimed in claim 23,  
wherein the catalytically active composition  
comprises promoters.

Claim 34. (Previously Presented).

The process as claimed in claim 23,  
wherein the catalyst support used is at least one  
material selected from the group consisting of cordierite,  
silicate, silicon dioxide, silicon carbide, aluminum oxide,  
aluminate, metal and metal alloy.

Claim 35. (Previously Presented).

The process as claimed in claim 23,  
wherein a catalyst support body used is selected  
from the group consisting of a honeycomb, a support having  
open cross-channel structure, a support having closed cross  
channel structure, and mixtures thereof.

Claim 36. (Previously Presented).

The process as claimed in claim 35, wherein  
wherein the catalyst support body used is a  
honeycomb having a cell density of a number of channels, of  
from 100 to 400 csi (cells per square inch).

Claim 37. (Previously Presented).

A method for preparing phthalic anhydride comprising  
a gas-phase oxidation reaction of o-xylene by  
contacting said o-xylene with a monolithic supported catalyst  
obtainable by the process as claimed in claim 23 in an  
adiabatic reactor in combination with an isothermally  
operated reactor.

Claim 38. (Previously Presented).

A method for preparing phthalic anhydride comprising  
a gas-phase oxidation reaction of naphthalene by  
contacting said naphthalene with a monolithic supported  
catalyst obtainable by the process as claimed in claim 23 in  
an adiabatic reactor in combination with an isothermally

operated reactor.

Claim 39. (Previously Presented).

A method for preparing phthalic anhydride comprising  
a gas-phase oxidation reaction of a mixture of o-xylene and naphthalene by contacting said mixture of o-xylene and naphthalene with a monolithic supported catalyst obtainable by the process as claimed in claim 23 in an adiabatic reactor in combination with an isothermally operated reactor.

Claim 40. (Previously Presented).

The method as claimed in claim 37,  
wherein the adiabatic reactor has upstream gas cooling in combination with an isothermally operated reactor.

Claim 41. (Previously Presented).

The method as claimed in claim 37,  
wherein the adiabatic reactor has upstream gas cooling, where gas cooling and the reaction are carried out

in a joint apparatus, in combination with an isothermally operated reactor.

Claim 42. (Previously Presented).

The method as claimed in claim 37,

wherein the adiabatic reactor has upstream gas cooling and downstream gas cooling, where gas cooling and the reaction are carried out in a joint apparatus, in combination with an isothermally operated reactor.

Claim 43. (Currently Amended).

A monolithic catalyst comprising

a catalyst support coated with a suspension; and said suspension comprises a catalytically active composition comprising

at least one type of  $TiO_2$  and 1-10% by weight of at least one surfactant of the formula



where R is a hydrophobic group of the surfactant and n is 1, 2 or 3; Y is a hydrophilic group of the surfactant and m is 0, 1, 2 or 3, and X is a hydrophilic head group of the



surfactant; and

the percent by weight is based upon the total composition weight; and

wherein the head group X present in the surfactant is a functional group selected from the group consisting of carboxylate, polycarboxylate, phosphate, phosphonate, sulfate and sulfonate;

wherein hydrophobic groups R of the surfactant used are selected from the group consisting of saturated alkyl radicals with carbon building blocks having from 5 to 30 carbon atoms, unsaturated alkyl radicals with carbon building blocks having from 5 to 30 carbon atoms; and

branched alkyl radicals with carbon building blocks having from 5 to 30 carbon atoms and are bound either directly or via aryl groups to a group selected from the group consisting of the hydrophilic group Y and the head group X.